

1.

(a)

$$\Delta T = 0 \rightarrow \Delta U = \Delta H = 0.$$

$$\Delta S = R \ln \frac{V_2}{V_1} = R \ln 2. \quad \Delta G = \Delta H - \Delta(TS) = -T\Delta S = -RT \ln 2, \quad \Delta F = \Delta U - \Delta(TS) = -T\Delta S = -RT \ln 2.$$

(b)

$$\Delta U = C_V \Delta T = C_V \cdot (T_2 - T_1), \quad \Delta H = C_p \Delta T = C_p (T_2 - T_1).$$

$$Q = 0 \rightarrow \Delta S = 0.$$

$$\Delta F = \Delta U - \Delta(TS) = \Delta U - T\Delta S - S\Delta T = C_V (T_2 - T_1) - S(T_2 - T_1) \Rightarrow \text{need absolute value of the entropy.}$$

$$\Delta G = \Delta H - \Delta(TS) = \Delta H - T\Delta S - S\Delta T = C_p (T_2 - T_1) - S(T_2 - T_1)$$

(c)

$$\Delta U = C_V \Delta T = C_V \cdot (T_2 - T_1), \quad \Delta H = C_p \Delta T = C_p (T_2 - T_1).$$

$$\Delta S = \int \frac{C_p}{T} dT = C_p \ln \frac{T_2}{T_1},$$

$$\Delta F = \Delta U - T\Delta S - S\Delta T = (C_V - S)(T_2 - T_1) - T_2 C_p \ln \frac{T_2}{T_1}$$

$$\Delta G = \Delta H - T\Delta S - S\Delta T = (C_p - S)(T_2 - T_1) - T_2 C_p \ln \frac{T_2}{T_1}$$

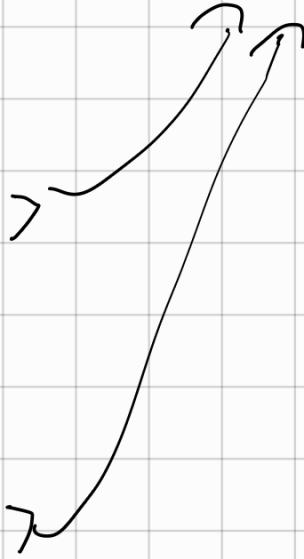
(d)

$$\Delta U = C_V \Delta T = C_V \cdot (T_2 - T_1), \quad \Delta H = C_p \Delta T = C_p (T_2 - T_1).$$

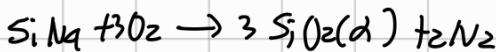
$$\Delta S = \int \frac{C_V}{T} dT = C_V \ln \frac{T_2}{T_1},$$

$$\Delta F = \Delta U - T\Delta S - S\Delta T = (C_V - S)(T_2 - T_1) - T_2 C_V \ln \frac{T_2}{T_1}$$

$$\Delta G = \Delta H - T\Delta S - S\Delta T = (C_p - S)(T_2 - T_1) - T_2 C_V \ln \frac{T_2}{T_1}$$



2.



$$\Delta H_{\text{exp}}^{\circ} = 3 \Delta H_{SiO_2}^{\circ} + 2 \Delta H_{N_2}^{\circ} - \Delta H_{Si(l)}^{\circ} - 3 \Delta H_{O_2}^{\circ} \quad \text{※ 표준상태 연산법}$$

$$= 3 \Delta H_{SiO_2}^{\circ} - \Delta H_{Si(l)}^{\circ}$$

$$= 3 \times -910.9 - -744.8 = -1988 \text{ kJ/mol.}$$

$$\Delta S_{\text{exp}}^{\circ} = 3 \Delta S_{SiO_2}^{\circ} + 2 \Delta S_{N_2}^{\circ} - \Delta S_{Si(l)}^{\circ} - 3 \Delta S_{O_2}^{\circ}$$

$$= 3 \times 41.5 + 2 \times 91.1 - 113 - 3 \times 205 = -220.8 \text{ J/mol.K}$$

$$\Delta C_p = \sum n C_p = 3 C_p(SiO_2) + 2 C_p(N_2) - C_p(Si_{(l)}) - 3 C_p(O_2)$$

$$= 26.99 + 99.174 \times 10^{-3} T - 13.05 \times 10^5 T^{-2} \text{ (J/mol.K)}$$

$$\Delta H^{\circ} (\text{800K}) = \Delta H_{298}^{\circ} + \int_{298}^{800} \Delta C_p \cdot dT$$

$$= -1988 \times 10^3 + \int_{298}^{800} 26.99 + 99.174 \times 10^{-3} T - 13.05 \times 10^5 T^{-2} dT \quad \frac{1}{T} \frac{1}{T^{-1}}$$

$$= -1988 \times 10^3 + 26.99 \cdot (800) + \frac{99.174}{2} \times 10^{-3} (800^2 - 298^2) + \frac{13.05}{2} \times 10^3 \left( \frac{1}{800} - \frac{1}{298} \right)$$

$$= -2005 \times 10^3 \text{ (J)}$$

$$\Delta S^\circ(800\text{K}) = \Delta S^\circ(298\text{K}) + \int_{298}^{800} \frac{\Delta C_p}{T} dT$$

$$= -220.8 + \int_{298}^{800} \left( \frac{26.99}{T} + 99.74 \times 10^{-3} - 13.05 \times 10^5 T^{-3} \right) dT$$

$$= -220.8 + 26.99 \ln \frac{800}{298} + 99.74 \times 10^{-3} (800 - 298) + \frac{13.05 \times 10^5}{2} \left( \frac{1}{800^2} - \frac{1}{298^2} \right)$$

$$= -250 \text{ J/K}.$$

$$\Delta G^\circ = \Delta H^\circ - T \Delta S^\circ$$

$$= -2005 \times 10^3 - 800 \cdot -250 = -(805 \times 10^3) \text{ J/mol}$$

$$C_p = 0 \text{ J/K} \quad \Delta S^\circ = -220.8 \text{ J/K mol}.$$

$$\Delta G'^\circ = \Delta H^\circ - T \Delta S'^\circ$$

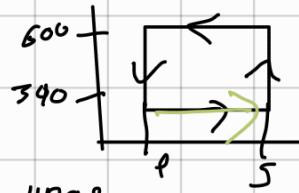
$$= -2005 \times 10^3 - 800 \cdot (-220.8) = -1828 \times 10^3 \text{ J/mol}$$

$$\text{error(\%)} = \frac{\Delta G'^\circ - \Delta G^\circ}{\Delta G^\circ} = \frac{-1828 + 805}{-1828} = 0.013 \text{ \%}$$

$$3, \text{ 1) } \Delta H^{\text{f} \rightarrow \text{s}}(590\text{K}) = -\Delta H_m(600\text{K}) + \int_{600}^{590} C_p(s) - C_p(T) dT.$$

$$= -4810 + \int_{600}^{590} -8.8 + 12.85 \times 10^{-3} T dT$$

$$= -4810 + (-8.8 \times -10) + \frac{12.85 \times 10^{-3}}{2} (590^2 - 600^2) = -4798$$



$$\Delta S^{\text{f} \rightarrow \text{s}}(590\text{K}) = \int_{600}^{590} \frac{C_p(s) - C_p(T)}{T} dT + \frac{\Delta H^{\text{f} \rightarrow \text{s}}}{T}$$

$$\approx \int_{600}^{590} \left( 12.85 \times 10^{-3} - \frac{8.8}{T} \right) dT - \frac{4810}{600}$$

$$= 12.85 \times 10^{-3} \cdot -10 - 8.8 \ln \frac{59}{60} - 8.01$$

$$\approx -8.00.$$

이때 브피변화, 암력변화가 0일 때까  $\Delta H$ 가 열의 양과 같거나 크다는 것을 알 수 있다.

$$\Delta S^{\text{f} \rightarrow \text{s}}_{\text{irr}}(590\text{K}) = \frac{Q}{T} = \frac{-\Delta H^{\text{f} \rightarrow \text{s}}(590\text{K})}{T} = \frac{4798}{590} = 8.13(\text{J})$$

$$\Delta S_{\text{tot}} = 0.13 > 0 \text{로 자발적인 반응.}$$

2)

$$\Delta G = \Delta H - T\Delta S$$

$$\Delta G^{\text{f} \rightarrow \text{s}}(590\text{K}) = \Delta H^{\text{f} \rightarrow \text{s}} - T\Delta S^{\text{f} \rightarrow \text{s}} \text{ at } 590\text{K.}$$

$$= -4798 + 8.00 \times 590 = -1850$$

$$\Delta G > 0 \text{ 으로 자발적 반응.}$$

3)

$$\begin{aligned} \Delta H^{\text{f} \rightarrow \text{s}}(550\text{K}) &= -\Delta H_m(600\text{K}) + \int_{600}^{550} C_p(s) - C_p(T) dT \\ &= -4810 + \int_{600}^{550} -8.8 + 12.85 \times 10^{-3} T dT \\ &= -4810 + -8.8 \times -50 + \frac{12.85 \times 10^{-3}}{2} (550^2 - 600^2) \\ &= -4739 (\text{J}) \end{aligned}$$

$$\begin{aligned} \Delta S^{\text{f} \rightarrow \text{s}}(550\text{K}) &= \int_{600}^{550} \frac{C_p(s) - C_p(T)}{T} dT + \frac{\Delta H^{\text{f} \rightarrow \text{s}}}{T} \\ &= \int_{600}^{550} \left( 12.85 \times 10^{-3} - \frac{8.8}{T} \right) dT - \frac{4810}{600} \\ &= 12.85 \times 10^{-3} \times -50 - 8.8 \ln \frac{55}{60} - 8.01 \\ &= -7.89 (\text{J}) \end{aligned}$$

$$\Delta S_{\text{irr}}(550\text{K}) = \frac{-4739}{550} = 8.61 (\text{J})$$

$$\Delta S_{\text{tot}} = 0.73 (\text{J})$$

$$\Delta S_{\text{tot}}(550\text{K}) > \Delta S_{\text{tot}}(590\text{K})$$

즉 550K에서 590K에 irreversible한 반응이 일어난다.

7)

✓  $\Delta G$ 로  $\Delta H$ 가 치숙값을 가지는 시점에서 평형이 일어난다.

$\Delta S$ 는  $\Delta S$ 를 통해  $\Delta G$ 의 부정이 가역적, 비가역적, 임은 알 수 있다

4.

단열된 통기장 안에 있으면  $\Delta H^{\text{e} \rightarrow \text{s}}$ 로 발생한 열이 계 안에 흐른다.

따라서 평형상태에서 liquid와 solid가 공존할 수 있다. 이때 그의 농도비는  $X_1$ 과 같고.

