

Numerical Method

Dept. Material Science & Engineering
Undergraduate Course (4th year)
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Midterm

Regression -> Non-linear Equation System

Data

- Gibbs Energy in pure Ps, Ks
- Enthalpy of Mixing in Liquid
- Activity of Ks in 1500K, Liquid
- Enthalpy of Formation in FCC, BCC
- Activity of Ps in BCC in 1100K
- Activity of Ks in FCC in 1100K

Equation System

- $\mu_L = \mu_{FCC}$
- $\mu_{FCC} = \mu_{BCC}$
- $\mu_L = \mu_{BCC}$
- Change of Temperature
- Binary System

Phase Diagram

Value of L_0, L_1
Temperature-dependent
Sub-regular Solution

Chemical Potential

- Liquid, FCC, BCC Phase
- Ps, Ks

Equation System

- X_L, X_{FCC}, X_{BCC} , Temperature
- $\mu_L = \mu_{FCC} = \mu_{BCC}$ of Ps, Ks
- "Triple Point"

Midterm

Thermodynamics

Enthalpy of Mixing

$$\begin{aligned}\Delta H_m &= \Omega X_{Ps} X_{Ks} \\ &= L X_{Ps} X_{Ks} && \text{(Regular)} \\ &= (L_0 + L_1 X_{Ks}) X_{Ps} X_{Ks} && \text{(Sub-regular)}\end{aligned}$$

$$L_0 = L_0^0 + L_0' T \quad L_1 = L_1^0 + L_1' T$$

Liquid Phase

- Enthalpy of Mixing

$$\frac{\Delta H_m^L}{X_{Ks}(1 - X_{Ks})} = L_0^0 + L_1^0 X_{Ks}$$

- Activity of Ks in Liquid

$$\frac{RT(\ln a_{Ks} - \ln X_{Ks})}{(1 - X_{Ks})^2} = L_0 + L_1 (2X_{Ks})$$

FCC Phase

- Enthalpy of Formation

$$\frac{\Delta H_f^{FCC} - \Delta G_{Ks}^{BCC \rightarrow FCC} X_{Ks}}{X_{Ks}(1 - X_{Ks})} = L_0^0 + L_1^0 X_{Ks}$$

- Activity of Ks in Liquid

$$\frac{RT(\ln a_{Ks} - \ln X_{Ks}) - \Delta G_{Ks}^{BCC \rightarrow FCC}}{(1 - X_{Ks})^2} = L_0 + L_1 (2X_{Ks})$$

BCC Phase

- Enthalpy of Formation

$$\frac{\Delta H_f^{BCC} - \Delta G_{Ps}^{FCC \rightarrow BCC} (1 - X_{Ks})}{X_{Ks}(1 - X_{Ks})} = L_0^0 + L_1^0 (1 - X_{Ks})$$

- Activity of Ps in BCC

$$\frac{RT(\ln a_{Ks} - \ln(1 - X_{Ks})) - \Delta G_{Ps}^{FCC \rightarrow BCC}}{(X_{Ks})^2} = L_0 + L_1 (2(1 - X_{Ks}))$$

Midterm

Regression

Enthalpy of Mixing

```
Y = <14894.230619> + <-4794.925467>x  
L_0 : 14894.230619  
L_1 : -4794.925467  
Sum of Square : 203.587186  
Value of R : 1.000000
```

Activity of Ks in liquid <1500K>

```
Y = <2907.183224> + <-9623.610085>x  
L_0 : 2907.183224  
L_1 : -9623.610085  
Sum of Square : 7261.723440  
Value of R : 0.999983
```

Enthalpy of formation in FCC

```
Y = <12597.609462> + <-7199.977924>x  
L_0 : 12597.609462  
L_1 : -7199.977924  
Sum of Square : 55.331968  
Value of R : 1.000000
```

Activity of Ks in fcc <1100K>

```
Y = <7100.938341> + <-14350.309179>x  
L_0 : 7100.938341  
L_1 : -14350.309179  
Sum of Square : 8305.546419  
Value of R : 0.999973
```

Enthalpy of formation in BCC

```
Y = <7000.896856> + <-6.654231>x  
L_0 : 7000.896856  
L_1 : -6.654231  
Sum of Square : 94.573085  
Value of R : 0.999155
```

Activity of Ps in BCC <1100K>

```
Y = <2688.598526> + <-155.708176>x  
L_0 : 2688.598526  
L_1 : -155.708176  
Sum of Square : 40726.904212  
Value of R : 0.008030
```

Liquid Phase

- $14894.2 - 7.99137T + (-4794.9 - 0.0112334T) X$

FCC Phase

- $12597.6 - 4.99703T + (-7199.98 + 0.0224905T)X$

BCC Phase

- Sub-regular model -> X
- Regular Model
- $7000.89 - 6.65423T$

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Chemical Potential

Reference State : Ks -> BCC
Ps -> FCC

Liquid Phase

$$\mu_{Ks}^L = \Delta G_{Ks}^{BCC \rightarrow L} + RT \ln X_{Ks} + (1 - X_{Ks})^2 (L_0^L + 2X_{Ks}L_1^L)$$

$$\mu_{Ps}^L = \Delta G_{Ps}^{FCC \rightarrow L} + RT \ln(1 - X_{Ks}) + X_{Ks}^2 (L_0^L + (2X_{Ks} - 1)L_1^L)$$

FCC Phase

$$\mu_{Ks}^{FCC} = \Delta G_{Ks}^{BCC \rightarrow FCC} + RT \ln X_{Ks} + (1 - X_{Ks})^2 (L_0^{FCC} + 2X_{Ks}L_1^{FCC})$$

$$\mu_{Ps}^{FCC} = RT \ln(1 - X_{Ks}) + X_{Ks}^2 (L_0^{FCC} + (2X_{Ks} - 1)L_1^{FCC})$$

BCC Phase

$$\mu_{Ks}^{BCC} = RT \ln X_{Ks} + (1 - X_{Ks})^2 (L_0^{BCC} + 2X_{Ks}L_1^{BCC})$$

$$\mu_{Ps}^{BCC} = \Delta G_{Ps}^{FCC \rightarrow BCC} + RT \ln(1 - X_{Ks}) + X_{Ks}^2 (L_0^{BCC} + (2X_{Ks} - 1)L_1^{BCC})$$

Liquid - FCC

$$\mu_{Ks}^L - \mu_{Ks}^{FCC} = 0$$

$$\mu_{Ps}^L - \mu_{Ps}^{FCC} = 0$$

FCC - BCC

$$\mu_{Ks}^{FCC} - \mu_{Ks}^{BCC} = 0$$

$$\mu_{Ps}^{FCC} - \mu_{Ps}^{BCC} = 0$$

Liquid - BCC

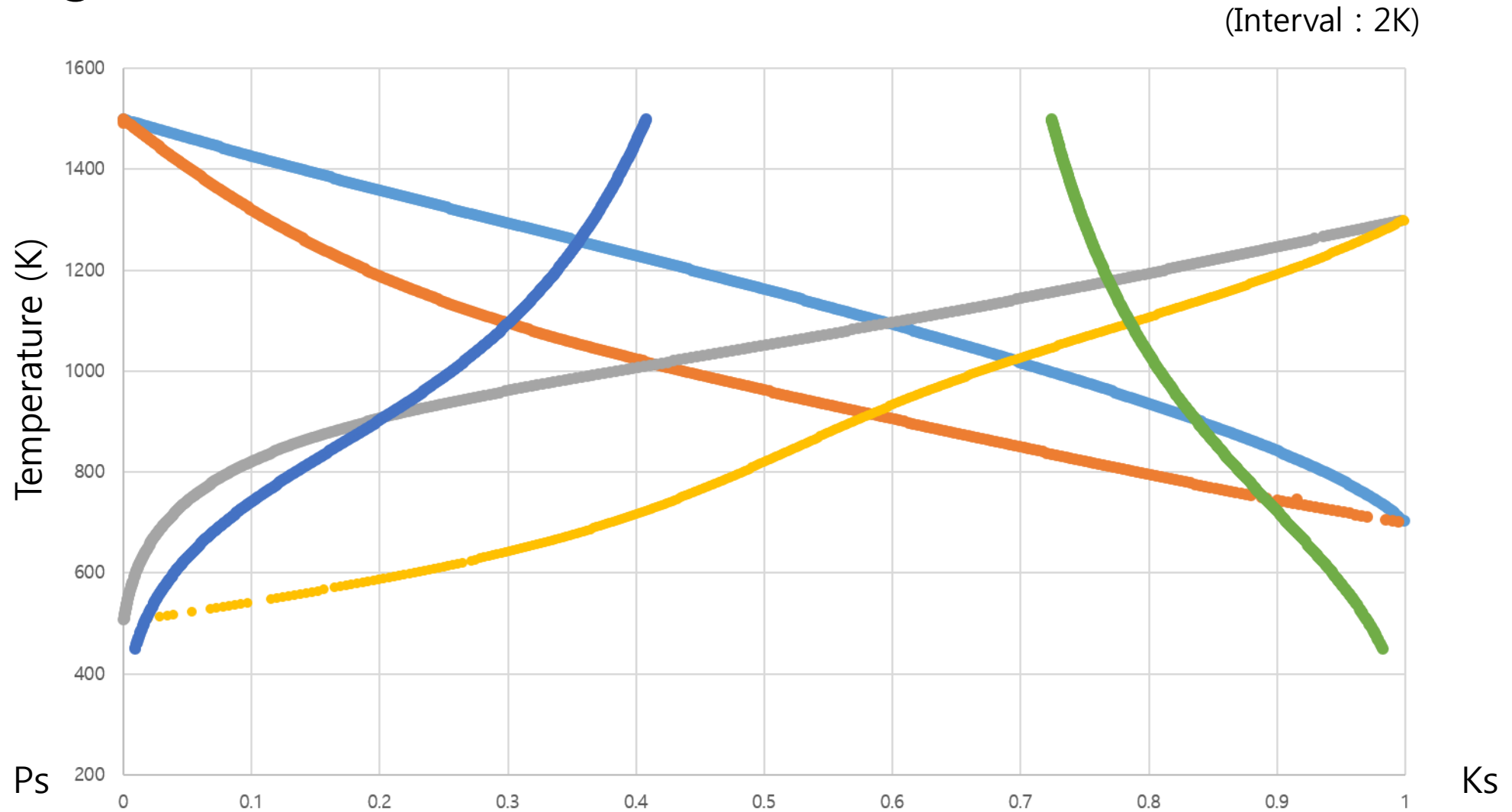
$$\mu_{Ks}^L - \mu_{Ks}^{BCC} = 0$$

$$\mu_{Ps}^L - \mu_{Ps}^{BCC} = 0$$

➡ Newton's Method

Midterm

Phase Diagram



Midterm

Chemical Potential

Triple Point

$$\mu_{Ks}^L = \mu_{Ks}^{FCC} = \mu_{Ks}^{BCC}$$

$$\mu_{Ps}^L = \mu_{Ps}^{FCC} = \mu_{Ps}^{BCC}$$

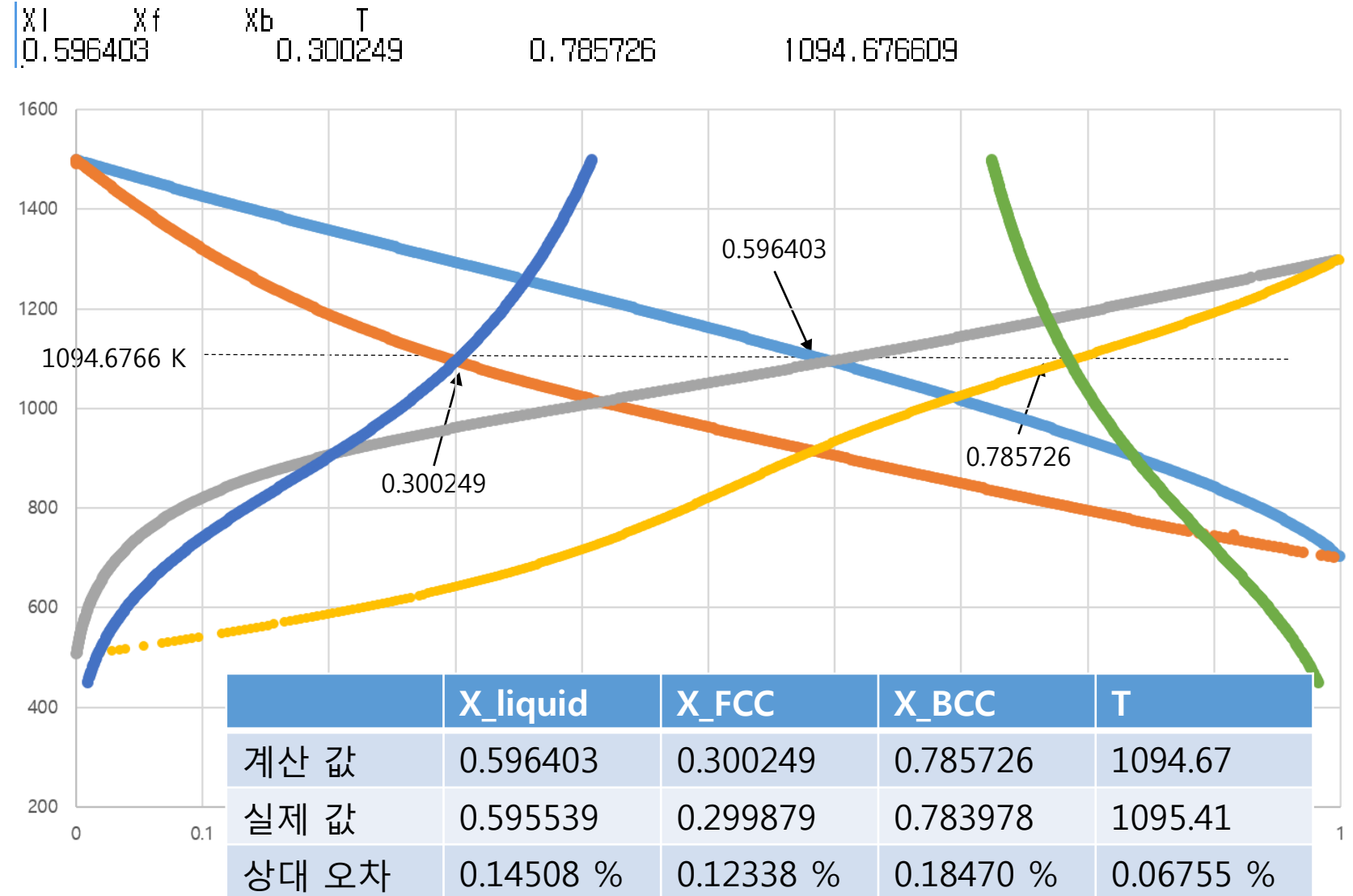


$$\mu_{Ks}^L - \mu_{Ks}^{FCC} = 0$$

$$\mu_{Ks}^L - \mu_{Ks}^{BCC} = 0$$

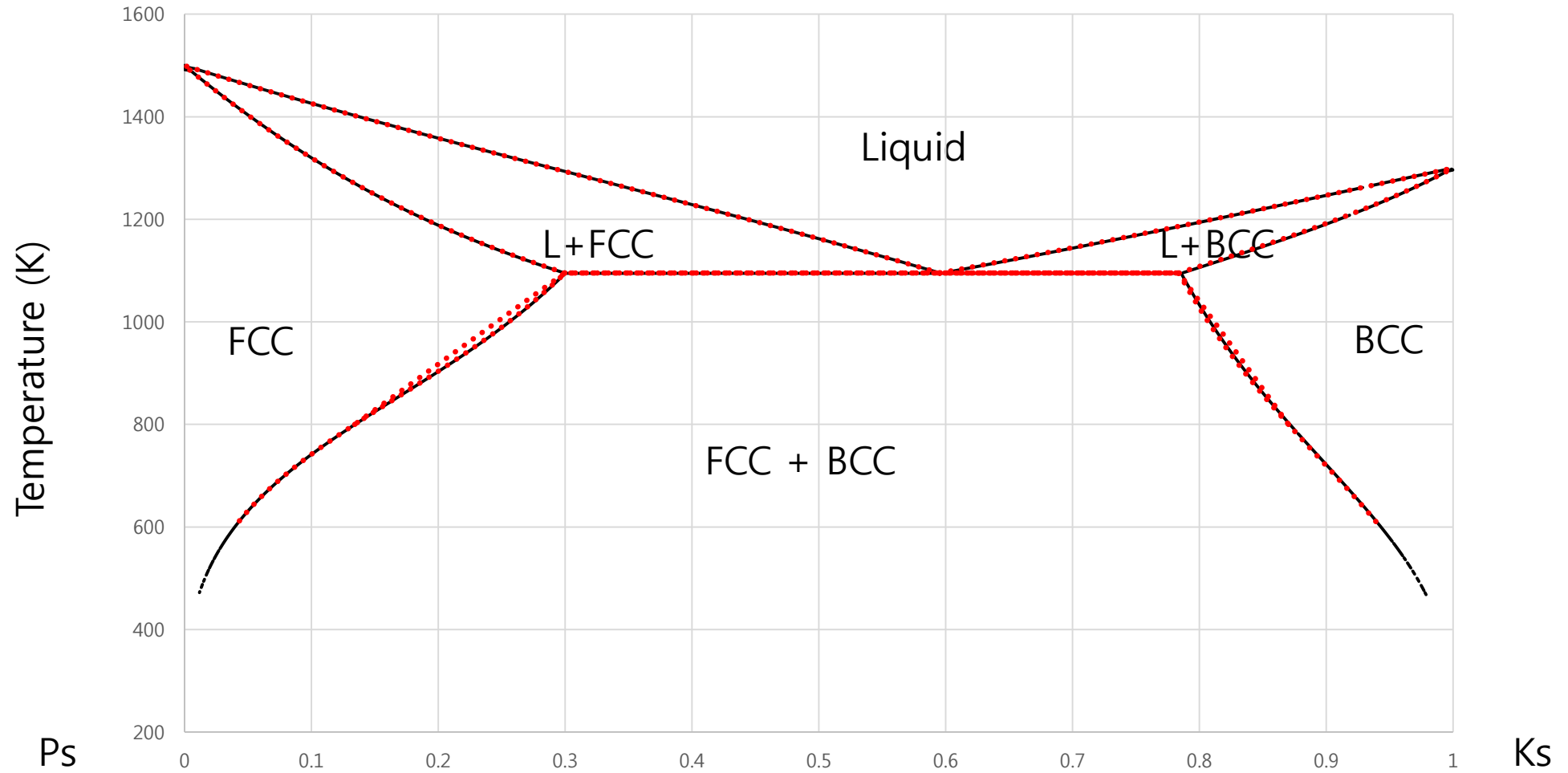
$$\mu_{Ps}^L - \mu_{Ps}^{FCC} = 0$$

$$\mu_{Ps}^L - \mu_{Ps}^{BCC} = 0$$



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Phase Diagram



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Code

```
#double CP_Ks_liq(double X_Ks, double T){ ... }
#double CP_Ps_liq(double X_Ks, double T){ ... }
#double CP_Ks_fcc(double X_Ks, double T){ ... }
#double CP_Ps_fcc(double X_Ks, double T){ ... }
#double CP_Ks_bcc(double X_Ks, double T){ ... }
#double CP_Ps_bcc(double X_Ks, double T){ ... }
#double **jacobian_liq_fcc(double X_l, double X_f, double T){ ... }
#double **jacobian_fcc_bcc(double X_f, double X_b, double T){ ... }
#double **jacobian_liq_bcc(double X_l, double X_b, double T){ ... }
#double *newton_method_liq_fcc(double Xl_ini, double Xf_ini, double T){ ... }
#double *newton_method_fcc_bcc(double Xf_ini, double Xb_ini, double T){ ... }
#double *newton_method_liq_bcc(double Xl_ini, double Xb_ini, double T){ ... }
#double draw_liq_fcc(double X_ini, double T_ini){ ... }
#double **jacobian_triple(double X_l, double X_f, double X_b, double T){ ... }
#double *newton_method_triple(double Xl_ini, double Xf_ini, double Xb_ini, double T_ini){ ... }
```

Chemical Potential

Jacobian

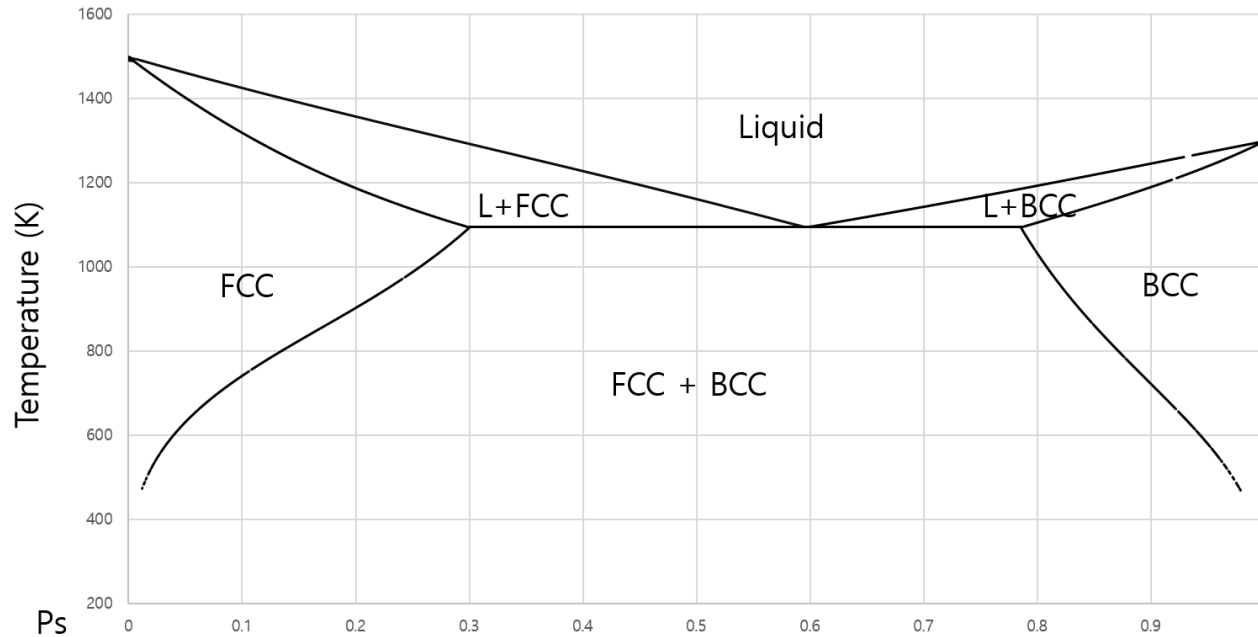
Newton Method

```
Jacob[0][0] = (R*T / X_l) - 2 * (L0_liq(T, 0) + 2 * L1_liq(T, 0) * X_l) * (1 - X_l) + 2 * L1_liq(T, 0)*pow((1 - X_l), 2);
Jacob[0][1] = -(R*T / X_f) + 2 * (L0_fcc(T, 0) + 2 * L1_fcc(T, 0) * X_f) * (1 - X_f) - 2 * L1_fcc(T, 0)*pow((1 - X_f), 2);
Jacob[0][2] = 0;
Jacob[0][3] = -12.5 + R*(log(X_l) - log(X_f)) + ((L0_liq(T, 1) + 2*L1_liq(T, 1)*X_l)*pow((1-X_l), 2)) - ((L0_fcc(T, 1) + 2*L1_fcc(T, 1)*X_f)*pow((1-X_f), 2));
Jacob[1][0] = (R*T / X_l) - 2 * (L0_liq(T, 0) + 2 * L1_liq(T, 0) * X_l) * (1 - X_l) + 2 * L1_liq(T, 0)*pow((1 - X_l), 2);
Jacob[1][1] = 0;
Jacob[1][2] = -(R*T / X_b) + 2 * (L0_bcc(T, 0) + 2 * L1_bcc(T, 0) * X_b) * (1 - X_b) - 2 * L1_bcc(T, 0)*pow((1 - X_b), 2);
Jacob[1][3] = -12.5 + R*(log(X_l) - log(X_b)) + ((L0_liq(T, 1) + 2 * L1_liq(T, 1)*X_l)*pow((1 - X_l), 2)) - ((L0_bcc(T, 1) + 2 * L1_bcc(T, 1)*X_b)*pow((1 - X_b), 2));
Jacob[2][0] = -(R*T / (1 - X_l)) + 2 * (L0_liq(T, 0) + (2 * X_l - 1) * L1_liq(T, 0)) * (X_l)+2 * L1_liq(T, 0)*pow((1 - X_l), 2);
Jacob[2][1] = (R*T / (1 - X_f)) - 2 * (L0_fcc(T, 0) + (2 * X_f - 1) * L1_fcc(T, 0)) * (X_l)-2 * L1_fcc(T, 0)*pow((1 - X_f), 2);
Jacob[2][2] = 0;
Jacob[2][3] = -10 + R*(log(1-X_l) - log(1-X_f)) + ((L0_liq(T, 1) + (2*X_l - 1) * L1_liq(T, 1))*pow((X_l), 2)) - ((L0_fcc(T, 1) + (2*X_f - 1) * L1_fcc(T, 1))*pow((X_f), 2));
Jacob[3][0] = -(R*T / (1 - X_l)) + 2 * (L0_liq(T, 0) + (2 * X_l - 1) * L1_liq(T, 0)) * (X_l)+2 * L1_liq(T, 0)*pow((1 - X_l), 2);
Jacob[3][1] = 0;
Jacob[3][2] = (R*T / (1 - X_b)) - 2 * (L0_bcc(T, 0) + (2 * X_b - 1) * L1_bcc(T, 0)) * (X_b)-2 * L1_bcc(T, 0)*pow((1 - X_b), 2);
Jacob[3][3] = -10 + R*(log(1 - X_l) - log(1 - X_b)) + ((L0_liq(T, 1) + (2 * X_l - 1) * L1_liq(T, 1))*pow((X_l), 2)) - ((L0_bcc(T, 1) + (2 * X_b - 1) * L1_bcc(T, 1))*pow((X_b), 2));
```

```
Jacob[0][0] = (R*T / X_l) - 2 * (14894 - 7.99137*T + 2 * (-4794.92 - 0.0112334*T) * X_l) * (1 - X_l) + 2 * (-4794.92 - 0.0112334*T)*pow((1 - X_l), 2);
Jacob[0][1] = -(R*T / X_f) + 2 * ((12597.6 - 4.99703*T) + 2 * (-7199.97 + 0.0224905*T) * X_f) * (1 - X_f) - 2 * (-7199.97 + 0.0224905*T)*pow((1 - X_f), 2);
Jacob[0][2] = 0;
Jacob[0][3] = -12.5 + R*(log(X_l) - log(X_f)) + (((-7.99137) + 2 * (-0.0112334)*X_l)*pow((1 - X_l), 2)) - (((-4.99703) + 2 * (-0.0224905)*X_f)*pow((1 - X_f), 2));
Jacob[1][0] = (R*T / X_l) - 2 * (14894 - 7.99137*T + 2 * (-4794.92 - 0.0112334*T) * X_l) * (1 - X_l) + 2 * (-4794.92 - 0.0112334*T)*pow((1 - X_l), 2);
Jacob[1][1] = 0;
Jacob[1][2] = -(R*T / X_b) + 2 * (6995.65 - 3.91579*T + 2 * 0 * X_b) * (1 - X_b) - 2 * 0*pow((1 - X_b), 2);
Jacob[1][3] = -12.5 + R*(log(X_l) - log(X_b)) + (((-7.99137) + 2 * (-0.0112334)*X_l)*pow((1 - X_l), 2)) - (((-4.99703) + 2 * (-0.0224905)*X_f)*pow((1 - X_f), 2));
Jacob[2][0] = -(R*T / (1 - X_l)) + 2 * (14894 - 7.99137*T + (2 * X_l - 1) * (-4794.92 - 0.0112334*T)) * (X_l)+2 * (-4794.92 - 0.0112334*T)*pow((1 - X_l), 2);
Jacob[2][1] = (R*T / (1 - X_f)) - 2 * ((12597.6 - 4.99703*T) + (2 * X_f - 1) * (-7199.97 + 0.0224905*T)) * (X_l)-2 * (-7199.97 + 0.0224905*T)*pow((1 - X_f), 2);
Jacob[2][2] = 0;
Jacob[2][3] = -10 + R*(log(1 - X_l) - log(1 - X_f)) + (((-7.99137) + (2 * X_l - 1) * (-0.0112334))*pow((X_l), 2)) - (((-4.99703) + (2 * X_f - 1) * (-0.0224905))*pow((X_f), 2));
Jacob[3][0] = -(R*T / (1 - X_l)) + 2 * (14894 - 7.99137*T + (2 * X_l - 1) * (-4794.92 - 0.0112334*T)) * (X_l)+2 * (-4794.92 - 0.0112334*T)*pow((1 - X_l), 2);
Jacob[3][1] = 0;
Jacob[3][2] = (R*T / (1 - X_b)) - 2 * (6995.65 - 3.91579*T + (2 * X_b - 1) * 0) * (X_b)-2 * 0*pow((X_b), 2);
Jacob[3][3] = -10 + R*(log(1 - X_l) - log(1 - X_b)) + (((-7.99137) + (2 * X_l - 1) * (-0.0112334))*pow((X_l), 2)) - (((-4.99703) + (2 * X_b - 1) * (-0.0224905))*pow((X_b), 2));
```

Midterm

Question & Answer



	X_liquid	X_FCC	X_BCC	T
계산 값	0.596403	0.300249	0.785726	1094.67
실제 값	0.595539	0.299879	0.783978	1095.41
상대 오차	0.14508 %	0.12338 %	0.18470 %	0.06755 %

반성할 점

- L 값을 계산한 뒤 대입하니 된다. 하지만 그래도 계산량이 많은지, Liquid – FCC와 Liquid – BCC를 한번에 못한다. (하나씩 주석 처리하며 계산했다.)
- Newton's Method에서 값이 나오지 않은 부분을 처리할 방법을 보충해야 한다. Cubic Spline도 나쁘지 않다고 생각.
- FCC와 FCC+BCC 사이의 선에서 오차가 발생했다.